







Determination of the steam amount inside long, fine cavities

using absorption spectroscopy and computational fluid dynamics

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Overview

I. Background

II. Methods

- Absorption spectroscopy
- Computational fluid dynamics

III. Steam penetration in thin-walled channels

- Geometry pipe
- Results original 134 °C sterilization cycle
- Results adapted 134 °C sterilization cycle

IV. Steam penetration in hollow devices

- Geometry simplified MD
- Results

V. Conclusion





Background

- > Steam penetration into lumen is still not fully understood
 - Influence of the geometry and material of the MD (medical device)
 - Influence of condensation & re-evaporation on the steam penetration behavior
 - Influence of the sterilization cycle (pressure curve)
- Monitoring currently based on CIs/BIs
 - Feedback only after cycle completion
 - No precise quantitative data
 - → New method needed
- Aim: improve fundamental understanding
 - Optimize sterilization cycles
 - Support manufactures with MD designs

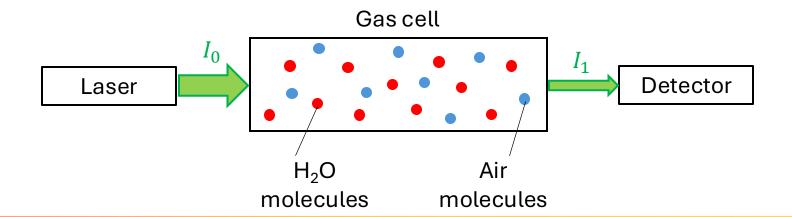






Absorption spectroscopy

- Water vapor interacts with light at specific wavelengths
 - Absorption occurs \rightarrow Intensity I is reduced ($I_1 < I_0$)
- As light source a tunable laser diode was used
 - at a wavelength of 1364 nm
 - wavelength tuned (changed) by current and temperature
- Photodetector measures the reduced light intensity I₁







Computational fluid dynamics

What is CFD:

- Powerful tool to simulate the fluid flow (liquids & gases) of real life applications
 - Aerodynamics around cars, combustions processes, etc.
 - > Steam penetration into cavities incl. condensation & evaporation effects

Why we use CFD in addition to experiments



Experiment

- provides real data
- but only at a few points

<u>CFD</u>

- Information of the entire domain
- Possible to investigate complex geometries

Together: Spectroscopy data ensures CFD is reliable

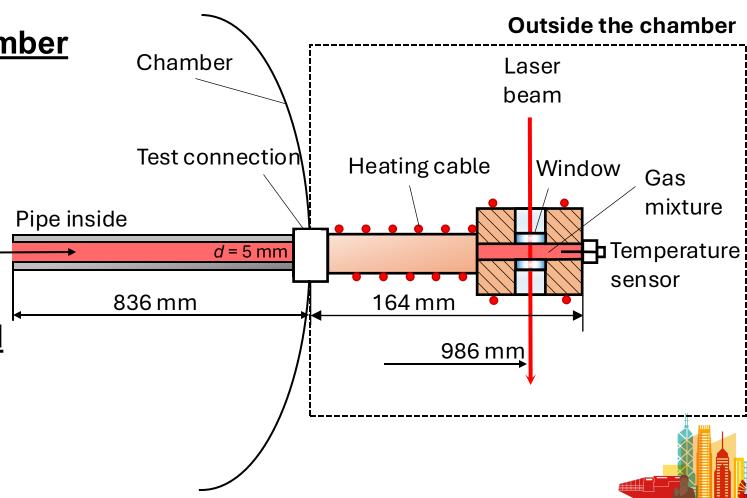


Optical setup outside the chamber

- heated to 140 °C (avoid condensation)
- heated "pipe" outside
 - aluminum
 - 164 mm long
 - 4 mm internal diameter
- Mountable to any autoclave via the test connection

1 meter long pipe investigated

- unheated pipe inside
 - stainless steel
 - 836 mm long
 - 5 mm internal diameter
 - 0.5 mm wall thickness





Sterilizer

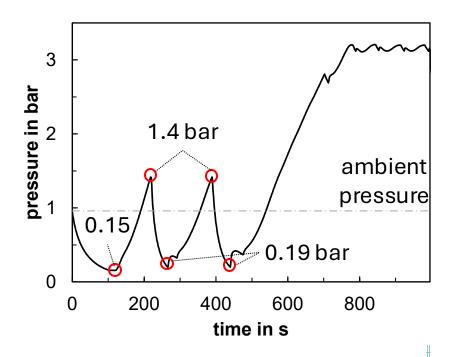
➤ Table top sterilizer – 22 liter chamber

Sterilization cycle

- Universal 134 °C
- ➤ 3 vacuum phases → setpoint 0.15 bar and 0.19 bar
- ≥ 2 pulsations → setpoint 1.4 bar

CFD simulation

- only internal pipe flow
- comparison of the H₂O mole fraction





Results of the 134 °C cycle

> At a depth of 986 mm

Comparison at the start of the sterilization plateau

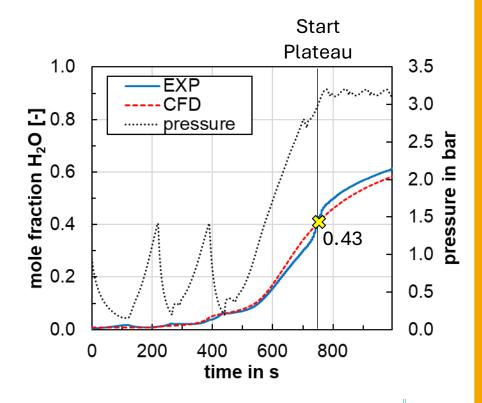
EXP: 0.43CFD: 0.42

Excellent agreement between experiment and simulation

Over the entire period

Similar low steam values also reported in:

"Steam penetration in thin-walled channels and helix shaped Process Challenge Devices", van Doornmalen et al. (2015)







Possibilities to increase steam penetration

- Increase number of pulsations
- Lower vacuum set points
- Higher injection set points

Leverage molecular diffusion

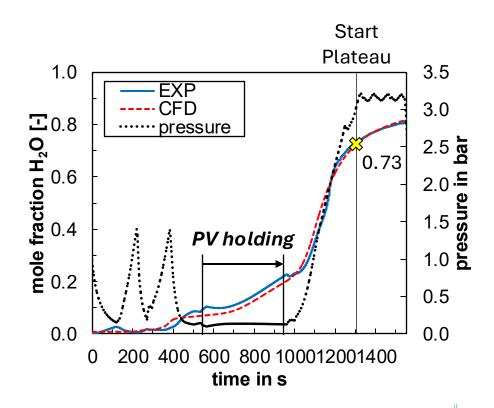
- The lower the pressure the stronger is this effect
- Similar to sterilization with hydrogen peroxide (H₂O₂)

"PV holding" phase introduced

- After the last vacuum phase
- 400 s at 0.13 bar

Steam amount increased to 0.73 (start plateau)

- Compared to 0.43 with the original cycle
- Hardly any additional water or energy required







Conclusion

Successfully measured the steam amount at the end of a 1 m pipe

- High temporal resolution (when happens what)
- Quantitatively resolved

CFD model matches experimental data excellently

Alternative cycle can be tested virtually

Steam penetration improves when adding holding phases during vacuum

- Steam amount increased from 0.43 → 0.73
- Requires almost no extra water or energy
- Trade-off: longer cycle time → "Eco-Mode"

Open Question: How much steam is needed inside cavities?

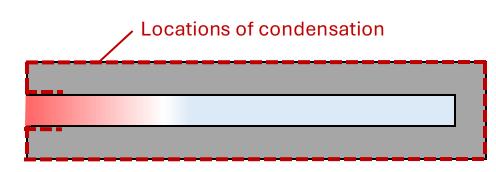
Future task: Combine our presented methods with Bls





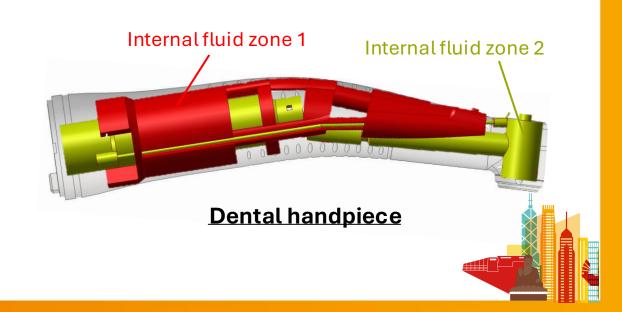
Steam penetration in thin-walled (metal) channels

- Condensation occurs mainly outside and slightly near the inlet
- > Internal surfaces heat up quickly due to thin walls
- Internal flow depends on pressure gradients and diffusion effects
- Phase changes can be neglected in the CFD modeling



Steam penetration in hollow devices

- Many internal surfaces to reach
- Outer walls heat up quickly
- > Inner walls remain cooler until steam enters
- Steam entry is essential to heat everything
- NCGs + condensation/re-evaporation strongly affect penetration





Steam penetration



hollow devices

Experiment to Validate the CFD

- Phase change strongly influences steam penetration
- ➤ Pipe around a pipe → "Double pipe"

Opening I

Main path to the optical measurement

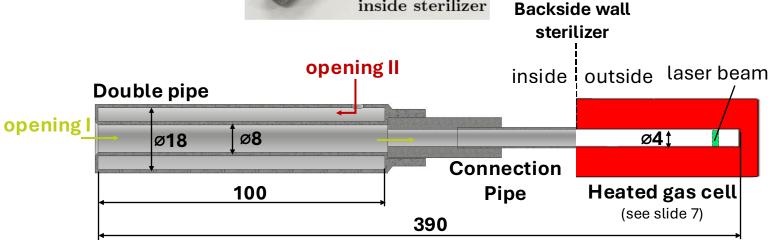
Opening II

Intermediate volume

For the optical measurement:

- Connection pipe mounted to the double pipe
- Both inside sterilizer
- On the outside: heated gas cell
- ➤ Internal length 390 mm







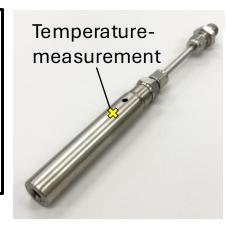


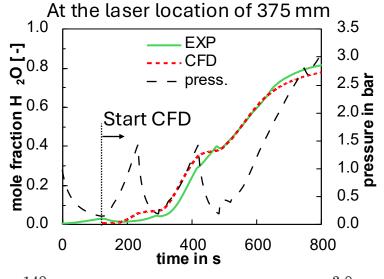
Results: steam penetration

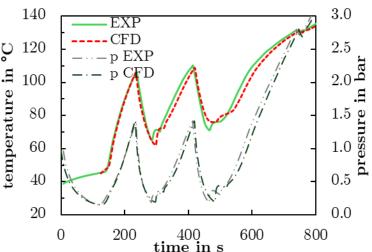
- Excellent agreement over the entire period
- Start of sterilization plateau (800s): only 0.03 difference in H₂O mole fraction

Results: temperature

- Temperature measurement during separate cycle
 - On the outside of the double pipe
- Excellent agreement over the entire period
 - Heating due to condensation
 - Cooling due to evaporation





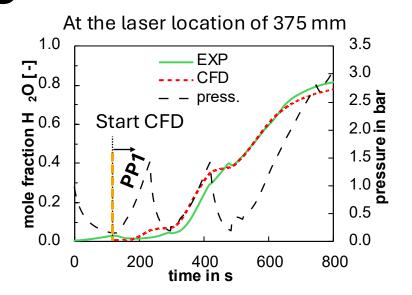


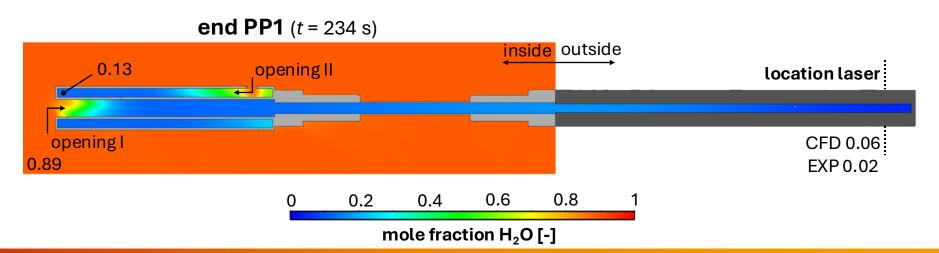




CFD: end PP1

- Hardly any steam penetration occurs
- Steam entirely condenses within the first 30 to 40 mm near both openings
- > Even though the **chamber environment** consists of **90** % **steam**

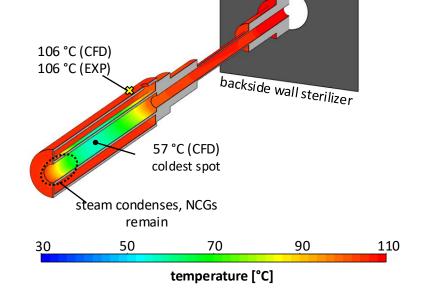




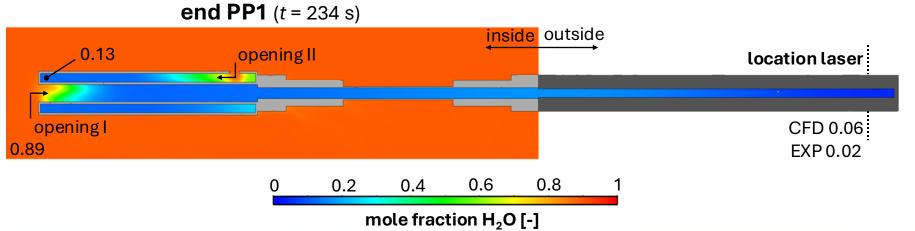


CFD: end PP1

- Hardly any steam penetration occurs
- Steam entirely condenses within the first 30 to 40 mm near both openings
- > Even though the **chamber environment** consists of **90** % **steam**
- Interior not well heated
 - Coldest spot is at 57 °C



end PP1 (t = 234 s)

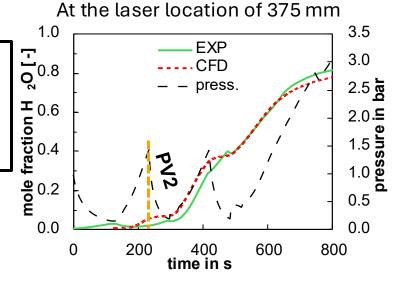


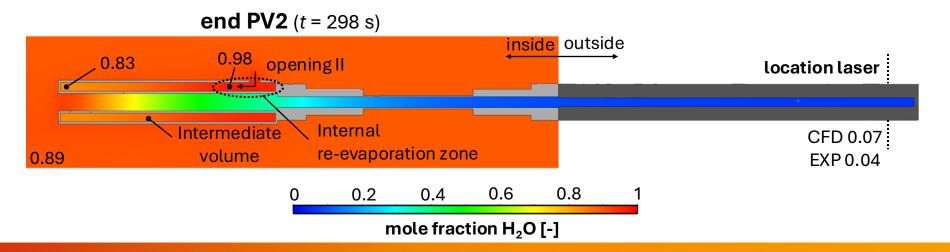




CFD: end PV2

- Huge increase in steam mole fraction in the intermediate volume
 - \triangleright 0.13 \rightarrow 0.83 from end of PP1 to end of PV2
 - > Driven by mass diffusion and re-evaporation near opening II

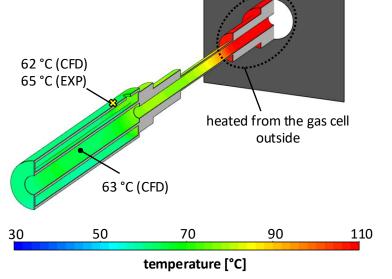




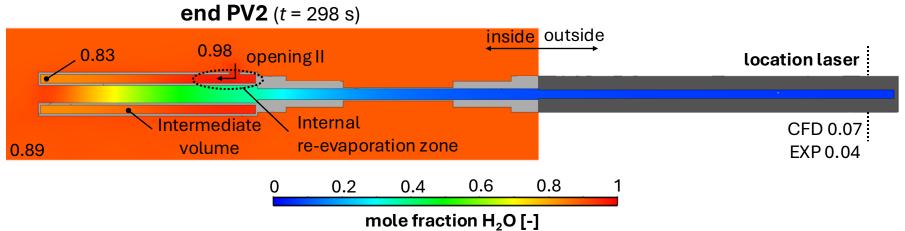


CFD: end PV2

- Huge increase in steam mole fraction in the intermediate volume
 - \triangleright 0.13 \rightarrow 0.83 from end of PP1 to end of PV2
 - Driven by mass diffusion and re-evaporation near opening II
- double pipe cools down to about 63 °C



end PV2 (t = 298 s)

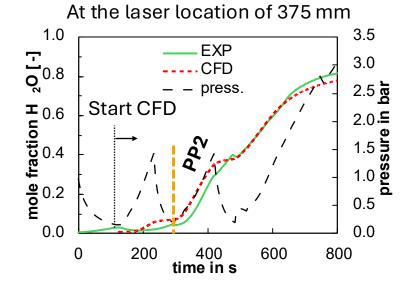


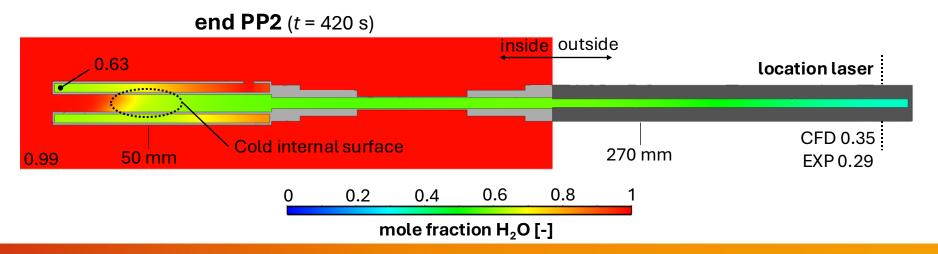




CFD: end PP2

- Cold internal surface acts as an unintended filter
 - ► H₂O mole fraction is around 0.55 between 50 mm and 270 mm
- Small amounts of NCGs cause this
 - About 1 % left in the chamber environment
- Create a 100 % steam environment!!!

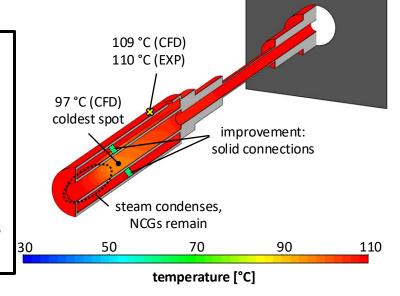




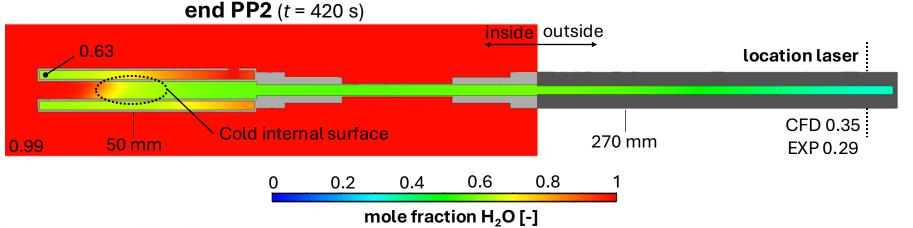


CFD: end PP2

- Cold internal surface acts as an unintended filter
 - > H₂O mole fraction is around 0.55 between 50 mm and 270 mm
- Small amounts of NCGs cause this
 - About 1 % left in the chamber environment
- Create a 100 % steam environment!!!
- Connect interior surfaces as well as possible with exterior surfaces
 - Heat conduction to the interior surfaces



end PP2 (t = 420 s)





Conclusion

- > Experiment & CFD: residual air strongly hinders steam penetration
 - Even with 99 % steam in the chamber, penetration into the MD failed
 - Goal: reach 100 % steam atmosphere as early as possible
 - Design rule: connect internal surfaces well with external surfaces
- > CFD successfully validated with experiments
 - Use it now for more complex device geometries
- Key questions CFD can answer:
 - Where and how much steam is present?
 - Where are the cold spots?
 - Is the load completely dry after the cycle?

Open Question: How much steam is needed inside cavities?

If everything is at the desired sterilization temperature





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Achieving more together I look forward to your ideas and questions

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Related peer-reviewed publications:

- **Publication I:** Steam penetration in long, narrow channels during steam sterilization: A combined study using wavelength modulation spectroscopy and CFD. https://doi.org/10.1002/cite.202200135
- Publication II: Modeling Steam Penetration into Hollow Devices: Effects of Phase Change and Non-Condensable Gases During Steam Sterilization. https://doi.org/10.1016/j.ijheatmasstransfer.2023.124396